### **GRADUALLY VARIED FLOWS**

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Gradually varied flows are open-channel flows whose water surface profile changes gradually. This means that, unlike rapidly varied flows, the hydrostatic pressure distribution is valid along the length of the flow. Both energy approach and momentum approach can be used for derivation, resulting in energy slope and friction slope, respectively. The two derivations provide different insights for gradually varied flows and understanding the difference between the two slopes is important. Features on some gradually varied flows are given and discussed

#### **1. Introduction**

*Gradually varied flow* is the steady flow whose water surface changes gradually along the length of the channel. This means two assumptions are involved in the definition: (1) the flow is steady - the hydraulic characteristics remain constant for the time interval and (2) the streamlines are practically parallel - the hydrostatic pressure distribution prevails over the channel section. *Varied flow* is the steady flow whose water surface changes gradually along the *i* the channel. This means two assumptions are involved in the definition: (1) the flow  $\tau$  - the hydraulic characteristics remain const **Example 10**<br>
string the steady flow whose water surface changes gradually along the<br>
c channel. This means two assumptions are involved in the definition: (1) the flow<br>
the hydraulic characteristics remain constant for t

# **2. Energy Approach**

Consider a control volume of water column in the figure below. The total head (*H*) is

$$
H = z + d\cos\theta + \alpha \frac{V^2}{2g} \tag{1}
$$

where  $z =$  elevation of a channel bottom from a certain datum,  $d =$  water depth normal to the water surface,  $\alpha$  = energy correction factor, and  $V =$  mean velocity. Assuming that  $\alpha = 1$ and the slope is very mild, then cos  $\theta \approx 1$  and  $d \approx y$  (water depth vertically from the bed).<br>
Substrainantly streamlines are practically parallel - the hydrostatic pressure distribution prevails over the<br>
channel secti Differentiating Eq.(1) with respect to *x* yields **e h e** *d* **d d e e d e d e e e d dider a control volume of water column in the figure below. The total head (***II***) is<br>**  $H = z + d \cos \theta + \alpha \frac{V^2}{2g}$  **(1)<br>**  $z =$  **elevation of a channel bottom from a certain datum,**  $d$  **= water depth normal to the<br>
surface,**  $\alpha$  **y Approach**<br>
a control volume of water column in the figure below. The total head (*H*) is<br>  $H = z + d \cos \theta + \alpha \frac{V^2}{2g}$  (1)<br>
= elevation of a channel bottom from a certain datum,  $d$  = water depth normal to the<br>
frace,  $\alpha$ 

$$
\frac{dH}{dx} = -S_e = -S_0 + \frac{dE_s}{dx} \tag{2}
$$

where  $S_e$  = the slope of the energy (grade) line. It should be noted in the above equation that the change of the total head (*dH*) is always negative (loss) in the flow direction. Yen and Wenzel (1970) showed that the slope of the energy line  $(S_e)$  is not the same as the friction slope  $(S_f)$  or the energy dissipation gradient, in general. Rewriting Eq.(2), we have

Gradually Varied Flow  
\n
$$
\frac{dE_s}{dx} = S_0 - S_e
$$
\n(3)  
\nwhich can be written as  
\n
$$
\frac{dy}{dx} = \frac{S_0 - S_e}{1 - Fr^2}
$$
\n(4)  
\nsince  
\n
$$
\frac{dE_s}{dx} = \frac{dE_s}{dy} \frac{dy}{dx}
$$
\n(5)  
\n
$$
\frac{dE_s}{dx} = 1 - Fr^2
$$
\n(6)  
\nEq.(4) is the governing equation for gradually varied flow, also referred to as "backwarder

which can be written as

$$
\frac{dy}{dx} = \frac{S_0 - S_e}{1 - Fr^2} \tag{4}
$$

$$
\frac{dE_s}{dx} = \frac{dE_s}{dy}\frac{dy}{dx} \tag{5}
$$

$$
\frac{dE_s}{dx} = 1 - Fr^2\tag{6}
$$

Gradually Varied Flo<br>  $\frac{dE_x}{dx} = S_0 - S_e$ <br>
(3)<br>
can be written as<br>  $\frac{dy}{dx} = \frac{S_0 - S_e}{1 - Fr^2}$ <br>  $\frac{dE_x}{dx} = \frac{dE_x}{dy} \frac{dy}{dx}$ <br>
(5)<br>  $\frac{dE_x}{dx} = 1 - Fr^2$ <br>
(6)<br>
is the governing equation for gradually varied flow, also referred Eq.(4) is the governing equation for gradually varied flow, also referred to as "backwater equation." It describes the variation of the flow depth <u>in a channel of arbitrary shape</u>.<br>Gradually varied flow should imply that the water depth does not change significantly in order to satisfy  $dA/dy = T$  in deriving  $dE_s/dx = 1 - Fr^2$ . (4)<br>(5)<br>(6)<br>gradually varied flow, also referred to as "backwater<br>of the flow depth <u>in a channel of arbitrary shape</u>.<br>that the water depth does not change significantly in<br> $dE_s/dx = 1 - Fr^2$ .



Figure 1. Flow in a rectangular prismatic open-channel

Yen and Wenzel (1970) presented a rigorous derivation of the governing equation for the spatially varied flow using the energy approach. For the case without the lateral inflow, the equation is given by Gradually Varied Flow<br>
Ind Wenzel (1970) presented a rigorous derivation of the governing equation for the<br>
Ily varied flow using the energy approach. For the case without the lateral inflow, the<br>
on is given by<br>  $\frac{dy}{dx}$ 

$$
\frac{dy}{dx} = \frac{S_0 - S_E}{1 - \frac{\alpha V^2}{gD}}
$$

where  $S_F$  is the energy dissipation gradient defined by

$$
S_E=-\frac{1}{\gamma A V}\frac{dE}{dx}
$$

Gradually Varied Flow<br>
H Wenzel (1970) presented a rigorous derivation of the governing equation for the<br>
varied flow using the energy approach. For the case without the lateral inflow, the<br>
is given by<br>  $\frac{z}{t} = \frac{S_0 - S$ which accounts for the dissipation of the mechanical energy of the mean motion within the fluid volume due to the fluid viscosity and turbulence. Thus, it can be said that Eq.(4) is not obtained from the energy approach in a rigorous sense. However, herein, Eq.(4) is taken to be the outcome of the energy approach since the total head by Eq.(1) is related to the energy of the open-channel flow.

### **3. Momentum Approach**

The derivation of the gradually varied flow equation from the force balance provides a better insight of the weakness of the backwater equation in the applications. For example, hydrostatic pressure distribution, which is extremely critical in practice, cannot be seen in the derivation from the energy concept.

For the fluid element between sections 1 and 2, the change of momentum flux in the *x*-direction is

$$
\sum F = \beta \rho Q (V_2 - V_1) \tag{7}
$$

where  $\beta$  is the momentum correction factor. The RHS of Eq.(7) is given by

$$
\sum F = \beta \rho Q (V_2 - V_1)
$$
\n6. (7)

\n7. (7)

\n7. (7)

\n8. (8)

\n7. (7)

\n8. (8)

\n9. (9)

\n1. (10)

\n1. (2)

\n1. (3)

\n2. (4)

\n2. (5)

\n3. (6)

\n4. (7)

\n5. (8)

\n6. (9)

If one divides Eq.(8) by *dx* and takes the limit as *dx* approaches zero, then Eq.(7) becomes

Gradually Variable Flow  
\n
$$
\sum F = \beta \rho Q (V_2 - V_1)
$$
\n(7)  
\n9 is the momentum correction factor. The RHS of Eq.(7) is given by  
\n
$$
\sum F = \gamma S_0 A dx - \tau_0 P dx - \int_A p dA \Big|_1^2
$$
\n(8)  
\n
$$
\text{vides Eq.(8) by } dx \text{ and takes the limit as } dx \text{ approaches zero, then Eq.(7) becomes}
$$
\n
$$
\gamma S_0 A - \tau_0 P - \frac{d}{dx} \int p dA = \beta \rho Q \frac{dV}{dx}
$$
\n(9)  
\n10  
\n10  
\n10

where the third term on the LHS is given by

$$
\int pdA = K\gamma A y \cos \theta \tag{10}
$$

*Fr* =  $\beta \rho Q(V_2 - V_1)$  (7)<br> *i* is the momentum correction factor. The RHS of Eq.(7) is given by<br>  $\sum F = \gamma S_0 A dx - \tau_0 P dx - \int_A \rho dA \Big|_1^2$  (8)<br>
vides Eq.(8) by dx and takes the limit as dx approaches zero, then Eq.(7) becomes<br> where  $K$  is the pressure coefficient. Note that even if the pressure distribution is hydrostatic, the value of *K* varies with the cross sectional shape and is  $K = 0.5$  only for a 2D flow. By using such relationships as vides Eq.(8) by dx and takes the limit as dx approaches zero, then Eq.(7) becomes<br>  $yS_0A - \tau_0P - \frac{d}{dx}\int pdA = \beta \rho Q \frac{dV}{dx}$  (9)<br>
third term on the LHS is given by<br>  $\int pdA = K\gamma A y \cos \theta$  (10)<br>
is the pressure coefficient. Note th les Eq.(8) by dx and takes the limit as dx approaches zero, then Eq.(7) becomes<br>  $d_0A = \tau_0 P - \frac{d}{dx} \int p dA = \beta \rho Q \frac{dV}{dx}$  (9)<br>
hird term on the LHS is given by<br>  $dA = K \gamma A y \cos \theta$  (10)<br>
the pressure coefficient. Note that even Eq.(8) by dx and takes the limit as dx approaches zero, then Eq.(7) becomes<br>  $-\tau_0 P - \frac{d}{dx} \int p dA = \beta \rho Q \frac{dV}{dx}$  (9)<br>
d term on the LHS is given by<br>  $= K \gamma A y \cos \theta$  (10)<br>
pressure coefficient. Note that even if the pressure d e third term on the LHS is given by<br>  $\int pdA = K \gamma A y \cos \theta$  (10)<br>
is the pressure coefficient. Note that even if the pressure distribution is hydrostatic,<br>
of *K* varies with the cross sectional shape and is *K* = 0.5 only for *e* third term on the LHS is given by<br>  $\int pdA = K\gamma A y \cos \theta$  (10)<br>
is the pressure coefficient. Note that even if the pressure distribution is hydrostatic,<br>
of K varies with the cross sectional shape and is  $K = 0.5$  only for a pressure coefficient. Note that even if the pressure distribution is hydrostatic,<br>varies with the cross sectional shape and is  $K = 0.5$  only for a 2D flow. By<br>tionships as<br> $A \frac{dV}{dx} = 0$  from continuity (11)<br>from continui *is* the pressure coefficient. Note that even if the pressure distribution is hydrostatic,<br> *dof K* varies with the cross sectional shape and is  $K = 0.5$  only for a 2D flow. By<br> *dr* h relationships as<br>  $\frac{dA}{dx} + A \frac{dV}{dx$ ssure coefficient. Note that even if the pressure distribution is hydrostatic,<br>ties with the cross sectional shape and is  $K = 0.5$  only for a 2D flow. By<br>ships as<br> $\frac{dV}{dx} = 0$  from continuity (11)<br> $\frac{v}{dx}$ <br>titen as<br> $\theta($ the pressure coefficient. Note that even if the pressure distribution is hydrostatic,<br>
K varies with the cross sectional shape and is  $K = 0.5$  only for a 2D flow. By<br>
elationships as<br>  $\frac{M}{\alpha} + A \frac{dV}{dx} = 0$ <br>
from continu the pressure coefficient. Note that even if the pressure distribution is hydrostatic,<br>
f K varies with the cross sectional shape and is  $K = 0.5$  only for a 2D flow. By<br>
elationships as<br>  $\frac{dA}{dx} + A \frac{dV}{dx} = 0$  from contin

$$
V\frac{dA}{dx} + A\frac{dV}{dx} = 0
$$
 from continuity (11)

and

$$
\frac{dA}{dx} = \frac{A}{D}\frac{dy}{dx} \tag{12}
$$

Eq.(9) can be rewritten as

$$
\frac{dy}{dx}\left[K\cos\theta(1+\frac{y}{D})-\frac{\beta V^2}{gD}\right]=S_0-\frac{\tau_0}{\gamma R_h}-y\frac{d(K\cos\theta)}{dx}
$$
\n(13)

or

$$
\frac{dy}{dx} = \frac{S_0 - \tau_0 / \gamma R_h}{\cos \theta \lambda - \frac{\beta V^2}{gD}}
$$
 (14)  
\nλ = K  $\left(1 + \frac{y}{D}\right) + y \frac{dK}{dy}$  (15)  
\n
$$
\hat{\lambda} = K \left(1 + \frac{y}{D}\right) + y \frac{dK}{dy}
$$
 (15)  
\n
$$
\text{ing above equation, it is assumed that } \beta \text{ does not vary with } x. \text{ If the pressure}
$$
\n
$$
\text{A in the system of the system}
$$

where

$$
\lambda = K \left( 1 + \frac{y}{D} \right) + y \frac{dK}{dy}
$$
\n(15)

In deriving above equation, it is assumed that  $\beta$  does not vary with *x*. If the pressure distribution is hydrostatic, then  $\lambda$  is unity (Yen and Wenzel, 1970). Thus, finally, we have

Gradually Variable Flow  
\n
$$
\frac{dy}{dx} = \frac{S_0 - r_0 / \gamma R_h}{\cos \theta \lambda - \frac{\beta V^2}{gD}}
$$
\n(14)  
\n
$$
\lambda = K \left( 1 + \frac{y}{D} \right) + y \frac{dK}{dy}
$$
\n(15)  
\n
$$
\frac{dy}{dx} = \frac{S_0 - S_f}{\cos \theta \lambda - \frac{\beta V^2}{gD}}
$$
\n(16)

where

$$
S_f = \frac{\tau_0}{\gamma R_h} \tag{17}
$$

(Q) Prove that  $\lambda = 1$  for hydrostatic pressure distribution.

### **4. Energy Slope and Friction Slope**

In solving GVF problems, it is necessary to evaluate *S<sup>f</sup>* if the momentum equation is used and  $S_e$  if the energy equation is used. The friction slope given by Eq.(17) accounts for the resistance due to external boundary shear stress in the *x*-direction. This value, however, is usually not available and it should be estimated by other means. Common practice is to approximate  $S_f$  by using the resistance relationship such as

Gradually Varied Flow

\n
$$
S = \frac{n^2 V^2}{C_m^2 R_h^{4/3}}
$$
\n
$$
S = \frac{V^2}{C^2 R_h}
$$
\n
$$
S = \frac{fV^2}{8gR_h}
$$

 $gR_{h}$ 

 $8gR_h$ 

Gradually Varied Flow<br>  $S = \frac{r^2 V^2}{C^2 R_h^{4/3}}$ <br>  $S = \frac{J V^2}{C^2 R_h}$ <br>  $S = \frac{J V^2}{8 g R_h}$ <br>
This is based on the assumption of steady uniform flow where  $S_0 = S_w = S_y$ .<br>
Evaluation of energy slope  $S_e$  requires detailed measurem Evaluation of energy slope *S<sup>e</sup>* requires detailed measurements of flow depth and mean velocity, which is nearly impossible. Similarly, common practice again approximates *S<sup>e</sup>* by the above resistance relationships. However, the assumption of equating two or more gradients  $(S_f = S_e = S_H)$  is only an approximation although it is often sufficiently accurate for engineering purposes. nergy slope  $S_e$  requires detailed measurements of flow depth and mean<br>is nearly impossible. Similarly, common practice again approximates  $S_e$  by<br>tance relationships. However, the assumption of equating two or more<br> $e = S_{$ s nearly impossible. Similarly, common practice again approximates  $S_e$  by<br>ance relationships. However, the assumption of equating two or more<br> $-S_{H}$ ) is only an approximation although it is often sufficiently accurate fo *c* of energy stope *S<sub>e</sub>* requires detailed measurements of thow depth and mean<br>which is nearly impossible. Similarly, common practice again approximates *S<sub>e</sub>* by<br>*c* resistance relationships. However, the assumption of which is nearly impossible. Similarly, common practice again approximates  $S_e$  by<br>  $\alpha$  resistance relationships. However, the assumption of equating two or more<br>  $(S_f - S_e - S_H)$  is only an approximation although it is often

(Q) Why the energy slope is frequently looked upon as the friction slope?

# **5. Classifications of the Gradually Varied Flow**

The gradually varied flow equation becomes

$$
\frac{dy}{dx} = S_0 \frac{1 - (y_n / y)^{10/3}}{1 - (y_c / y)^3}
$$
(20)

if the Manning formula is used for the friction slope (or total head gradient). Similarly, we

have

Gradually Varied Flow  
\n
$$
\frac{dy}{dx} = S_0 \frac{1 - (y_n / y)^3}{1 - (y_c / y)^3}
$$
\n(21)\n  
\nexp formula is used.

if the Chezy formula is used.



Figure 11.20 Various types of nonuniform flow with flow from left to right.

Figure 2. Various flow profiles of gradually varied flows

#### **6. Some Flow Profiles**

# **6.1 Flow under the Sluice Gate**

The flow under the sluice gate on the mild slope is considered. The flow profile upstream of the gate is M1 curve. The flow from the tip of the gate shows a vena contracta because of the generation of the highly-curvilinear flow. Hydrostatic pressure distribution is not valid for this type of flow. Therefore, care must be taken when applying the energy equation. If the gate is located between the bed and  $y_c$ , the flow profile is M3 curve. Then, in order to go across the critical depth, the hydraulic jump should take place. If the jump rises to a height between  $y_c$  and  $y_n$ , then M2 curve is made. Or, if the jump rises to a height beyond  $y_n$ , then M1 curve is made. In both cases, the flow depth never approaches  $y_n$  far downstream. Therefore, the jump will rise exactly to  $y_n$ .



Figure 3. Flow under the sluice gate

### **6.2 Flow on the changing slope**

The flow on the mild slope is considered. If the slope increases slightly, then the normal depth is lowered accordingly, without changing the critical depth. The flow profile upstream

of the break in slope shows M2 curve. If the flow depth is located at a height higher than  $y_n$ , then M1 curve is made. Or, if the flow depth is located between  $y_c$  and  $y_n$ , then M2 curve is made. In both cases, the flow depth never approaches  $y_n$  far downstream. Therefore, the flow depth at the break in slope drops exactly to  $y_n$ .



Figure 4. Flow on the increasing slope

If the slope decreases slightly, then the normal depth is lifted accordingly but the critical depth does not change. The flow profile upstream of the break in slope shows M1 curve. If the flow depth is located at a height higher than  $y_n$ , then M1 curve is made. Or, if the flow depth is located between  $y_c$  and  $y_n$ , then M2 curve is made. In both cases, the flow depth never approaches  $y_n$  far downstream. Therefore, the flow depth at the break in slope increase exactly to  $y_n$ .



Figure 5. Flow on the decreasing slope

### **6.3 Flow on the slope changing roughness**

The flow in the channel whose roughness changes is considered. If the roughness downstream of the channel decreases significantly, then the normal depth can be located below the critical depth. This is due to that the critical slope is proportional to the square of **6.3 Flow on the slope changing roughness**<br>The flow in the channel whose roughness changes is considered. I<br>downstream of the channel decreases significantly, then the normal dept<br>below the critical depth. This is due to *c h S n gD R* <sup>=</sup> ). In this case, the flow profiles upstream and downstream of Section 1 are M curve and S curve, respectively. The flow profile upstream of Section 1 is M2, and the flow depth at Section 1 should be  $y_c$ . This is because, if the flow depth is higher than  $y_c$ , the flow profile is S1 curve and never approach  $y_n$ . If the flow depth is lower than  $y_c$ , then the flow profile is S2 curve and never approach  $y_n$  downstream of this section.



Figure 6. Flow on the slope changing roughness greatly

If the roughness downstream of the channel decreases slightly, then the normal depth is lowered but is higher than  $y_c$ . In this case, the both flow profiles upstream and downstream of Section 1 are M curves, and the flow depth at Section 1 is  $y_n$ . This is because, if the flow depth is higher than  $y_n$ , the flow profile is M1 curve and never approach  $y_n$ . If the flow depth is lower than  $y_n$ , then the flow profile is M2 curve and never approach  $y_n$ downstream of this section.



Figure 7. Flow on the slope changing roughness gently

#### **7. Methods of Computation**

Computation of gradually varied flow is important in hydraulic engineering practice. Recently, money for the compensation far exceeds money for the construction in building a dam. So accurate computation of the backwater equation under various circumstances is highly desired. Methods for computing the gradually varied flow can be divided into

(1) Direct integration method

- Bresse method
- Chow's method
- (2) Step method
	- Direct step method
	- Standard step method

(3) Numerical method

### **References**

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Yen, B.C., and Wenzel, H.G. (1970). "Dynamic equations for steady spatially varied flow." *Journal of the Hydraulics Division*, ASCE, 96(HY3), 801-814.

Sabersky, R.H., Acosta, A.J., and Hauptmann, E.G. (1971). *Fluid Flow*. Macmillan, New York, NY.

# **Problems**

# 1. **Gradually Varied Flow Profile** (Julien, p.49)

Consider steady flow in the following impervious rigid boundary channel. The discharge per unit width q is 3.72  $m^2/s$  and the water depth at the downstream dam site is 10 m. Assume that the channel width remains large and constant regardless of flow depth, and  $f = 0.03$ . Determine the distribution of the flow depth, mean velocity, and bed shear stress along the 25 km reach of the channel using the numerical method (Newton-Raphson method). Obtain the flow profiles using the following step methods and compare the results:

(a) direct step method

(b) standard step method

